

# PREPARATIVE AND INDUTRIAL SCALE ISOLATION AND PURIFICATION OF POLYUNSATURATED FATTY ACIDS (OMEGA-3 AND OMEGA-6)

How to Contact Us:
OS Pilot Plant Corporation
Saskatoon, SK, S7N 2R4
CANADA
http://www.pos.ca
Tel: (306) 978 2800
Fax: (306) 975 3766

## Udaya N. Wanasundara

#### INTRODUCTION

Long-chain omega-3 and omega-6 polyunsaturated fatty acids (PUFAs) have become an important subject in both the scientific community and our everyday life, and we encounter them in pharmaceutical and/or health applications as well as in food applications. Among these PUFA's have attracted especial attention, due to their role in human health and nutrition. Essential fatty acids cannot be synthesized de novo by humans and therefore, need to be obtained from the diet. With the growing public awareness of the nutritional benefits of PUFA's, the market for such products is expected to grow in the future. Docosahexaenoic (DHA), eicosapentaenoic (EPA) and gamma linoleic (GLA) acids are the mostly used PUFA in nutraceuticals and functional foods. They are being used in wide array of products ranging from dietary supplements to infant formulas.

Naturally these fatty acids are associated with other lipophilic compounds and effective separation and isolation techniques are needed to recover them in concentrated forms. With the growing public awareness of the nutritional benefits of PUFAs, the market for such products is expected to grow in the future. This presentation focuses on some of the new methodologies that we'll be able to provide in addition to the capabilities at present.

### Omega-3 (w3) and Omega-6 (w6) Fatty Acids

H<sub>3</sub>C  $\alpha$ -Linolenic acid (ALA 18:303)



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• Utilizes the melting point (MP) characteristic of fatty acids, which depends on chain length and degree of unsaturation.

• As the chain length increases, MP of fatty acids increases, however, for longer chain fatty acids, unsaturation, results in a decrease of MP.

 At low temperature, short chain fatty acids crystallize and PUFAs can be isolated from the rest of the fatty acids.

 Organic solvents (eg. Hexanes, Acetone) facilitate separation of fatty acids during crystallization.

LOW	Temperature Crystallization				
1	Enrichment of @3 Fatty	y Acids by	Low Temp	perature Cry	stallization

	Fatty Acid	Starting	Hexa	anes	Ace	tone	Conditions
	Esters	Oil	TAG	FFA	TAG	FFA	Marine oil (TAG or FFA)
	EPA (%)	6.8	8.2	11.8	12.0	13.8	Solvents: Hexanes or Acetone
	2()0)	0.0	0.2		.2.0	1010	Oil-to-solvent ratio: 1:4 (w/v)
	DHA (%)	8.4	10.1	12.5	15.1	17.5	Temperature: -25°C
Jacketed lank							Time: 24h with slow mixing
(Saturated fatty acids)	Total <b>ω3</b> (%)	22.2	27.8	31.6	37.2	40.6	Separate crystals by filtration
Non-crystallized fraction	n						Evaporate solvent from liquid
(FUFAS)							fraction (non-crystallized fraction)

 Fractional distillation uses the differences in the boiling point and molecular weight of fatty acid esters under vacuum (0.1-4.0 mmHg) and high temperatures (150-210°C).

• Table shows the conditions and results of fractional distilled marine oil ethyl esters (EE).

 By fractional distillation, more than doubling of the Omega-3 fatty acids in the isolate (nondistilled fraction) can be achieved.

#### Fractional Distillation

Enrichment of ω3 Fatty Acid-Ethyl Esters by Fractional Distillation									
Fatty Acid	Starting Marine Oil	<b>T</b> : 14	Tilo	Conditions	Trial-1	Trial-2			
	Laters	Trial-1	Trial-2	Temperature (°C)	170	190			
EPA-EE	7.0	11.8	11.8	Vacuum (mm Hg)	1.5	1.5			
DPA-EE	4.2	7.0	12.2		_	_	L		
DHA-EE	8.8	15.5	26.2	Holding Time (min)	1	/			
Total <b>@3</b> -EE	23.2	38.2	53.1						
Yield (%)		50	23						

• In a free fatty acid (FFA) mixture, saturated and monounsaturated fatty acids can be complexed with urea.

 Presence of double bonds increases the bulk of the molecule and reduces the likelihood of its complexation with urea, i.e. PUFAs remain in the liquid and are referred to as non-urea complexing fraction (NUCF).



Values	Algal	Borage	Flax	EPA	Marin	e
are in %	DHA	GLA	ALA		DPA	DHA
Starting oil After urea Urea-to-FFA Ratio (w/w)	57.1 98.8 <mark>4:1</mark>	21.8 88.1 <mark>3:1</mark>	57.2 80.1 <mark>2:1</mark>	6.8 10.9	4.2 2.4 <mark>3:1</mark>	8.4 67.6

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Urea Complexation